In the claims:

1.-2. (cancelled)

3. (previously amended) A method as recited in claim 18, wherein the gas stream has a temperature of from about 350°C to about 600°C.

4. (cancelled)

5. (previously amended) A method as recited in claim 18, wherein the ammonia/N_2O concentration ratio is up to about 2.0 based on the total volume of the gas stream.

6. (previously amended) A method as recited in claim 18, wherein the ammonia/N_2O concentration ratio is at least about 0.5 based on the total volume of the gas stream.

7. (previously amended) A method as recited in claim 18, wherein the ammonia/N_2O concentration ratio is from about 0.8 to about 1.0 based on the total volume of the gas stream.

8.-9. (cancelled)

10. (previously amended) A method as recited in claim 18, wherein the zeolite is ion-exchanged with at least one type of ion selected from the group consisting of Fe, Cu, Co, Ce, Pt, Rh, Pd, Ir, Mg and combinations thereof.

11. (previously amended) A method as recited in claim 18,wherein the zeolite is ion-exchanged with at least one type of ion selected from the group consisting of Fe, Ce, Cu, Co and combinations thereof.

12. (previously amended) A method as recited in claim 18, wherein the N_2O concentration of the gas stream is about 1% or less.

13. (previously amended) A method as recited in claim 18, wherein the N_2O concentration of the gas stream is about 5,000 ppm or less.

14. (previously amended) A method as recited in claim 18, wherein the N_2O concentration of the gas stream is between about 20 ppm and about 5,000 ppm.

15.-17. (cancelled)

18. (currently amended) A method for ammonia-mediated N_2O and NOx reduction, comprising contacting a gas stream containing N_2O and NOx with ammonia and a catalyst comprising a BETA zeolite which is selective for the simultaneous reduction of N_2O and NOx, wherein the gas stream containing ammonia, nitrous oxide and ~~nitrous oxide~~ NOx ~~and~~ has a temperature of greater than about 250°C.

19.-24. (cancelled)